Hydromagnetic Oscillatory Flow and Heat Transfer in Dusty Viscoelastic Fluid Through Porous Medium in an Inclined Channel in The Presence of Thermal Radiation and Heat Sink

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Abstract: In this study, the unsteady magnetohydrodynamic (MHD) flow and heat trasnfer of a dusty, viscoelastic, incompressible and electrically conducting fluid in an inclined channel in the presence of thermal radiation and heat source has been investigated. The non-dimensional equations governing the flow are solved by parametric perturbation technique under the prescribed boundary conditions. The solutions of the equations governing the flow are obtained for fluid velocity, dust particle velocity, temperature and dust particle temperature profile. The results have been expressed graphically and in tabular form to observe the effects of different flow parameters. The effect of the various parameters entering in the governing equations on the flow are evaluated numerically and discussed with the help of graphs and tables.

Keywords: Magnetohydrodynamics,, inclined channel, dusty and viscoelastic fluids.

Mathematical Subject Classification: 76A10, 76D99, 76S99, 76W99.

Introduction

Magnetohydrodynamics (MHD) convection flows of electrically conducting viscous incompressible fluids have gained significance in recent times owing to its applications in physics and engineering. In view of increasing technical applications using Magnetohydrodynamic effect, it is desirable to extend many of available viscous hydrodynamic solution to include the effect of magnetic field for those cases when the viscous fluid is electrically conducting. The study of heat transfer effects on magnetohydodynamics (MHD) free convection flow in porous medium is also highly important due to the significant contribution of magnetic field on the performance of many systems using electrically conducting fluids and on the boundary layer flow control. The magneto hydrodynamic heat transfer has gained considerable attention because of its applications in recent advancement of space technology. Greenspan and Carrier [1] have studied the Magnetohydrodynamics (MHD) flow past a flat plate. Unsteady MHD convective heat transfer past a semi-infinite vertical porous plate with variable suction have been investigated by Kim[2]. Attia and Kotab [3] have investigated the Magnetohydrodynamics (MHD)flow between two parallel plates with heat transfer. The effect of variable viscosity on hydromagnetic flow and heat transfer past a continuously moving porous boundary with radiation have been studied by Seddeek [4]. The effect of heat transfer to MHD oscillatory flow in a channel filled with a porous medium have been investigated by Makinde and Mhone [5]. Seth et.al. [6] have discussed the unsteady MHD convective flow within a parallel plate rotating channel with thermal source/sink in a porous medium under slip boundary conditions. MHD flow through rotating porous medium with radiating heat transfer in the presence of fluctuating thermal diffusion has studied by Sharma and Saini [7]. Singh [8] investigated the effect of injection/ suction on convective oscillatory flow through porous medium bounded by two vertical porous plates. The numerical study of convective heat transfer through porous medium in a vertical channel with radiation effect have been dealt by Kumar and Nath [9]. Abbas et.al.[10] analysed the heat transfer due to an unsteady stretching/shrinking cylinder with partial slip condition and suction. Heat transfer with radiation and

temperature dependent heat source in MHD free convection flow in a porous medium between two vertical wavy walls has been discussed by Dada and Disu [11].

All the above investigations are free from viscoelastic fluids. The heat transfer behaviour of viscoelastic fluid between parallel plates is of great interest in many fields, like; petroleum production, food preservation and power engineering. The effect of injection on the flow of second grade fluid in the inlet region of a channel has discussed by Mishra and Panda [13]. The flow viscoelastic fluid past a porous plate has been analyzed by Ariel [14]. Maneschy et. al [15] also studied the heat transfer analysis of a non-Newtonian fluid past a porous plate. Kurtcebe and Erim [16] have characterized the heat transfer of a visco-elastic fluid in a porous channel. Unsteady Couette flow with heat transfer in a visco elastic fluid considering the Hall Effect has been investigated by Hazem [17]. Sharma and Pareek [18] studied the effect of unsteady flow and heat transfer through an elastico-viscous liquid along an infinite hot vertical porous moving plate with variable free stream and suction. Visco elastic mixed convection MHD oscillatory flow through a porous medium filled in a vertical channel has been studied by Singh[19]. Choudhary and Jyoti [20] discussed the heat transfer to MHD oscillatory visco elastic flow in a channel filled with porous medium. The effects of variable viscosity on the peristaltic flow of non-newtonian fluid through a porous medium in an inclined channel with slip boundary conditions have been investigated by Khan and Usman [21]. Garg et.al. [22] give the analysis of an oscillatory MHD convective flow of viscoelastic fluid through porous medium filled in a rotating vertical porous medium filled in a rotating vertical porous channel with heat radiation.

In the present paper we consider the dusty viscoelastic fluid. A dusty viscoelastic fluid is the mixture of viscoelastic fluid and dust particles. The dusty fluid model is important due to its application in paper industry, industrial filtration, ceramic engineering, power metallurgy, smoke emission from vehicles, combustion, use of dust in gas cooling systems, centrifugal separation of matter from fluid, petroleum industry, purification of crude oil, electrostatic precipitation, polymer technology, and fluid droplets sprays. The volume of dust particles is generally assumed to be negligible in dynamics of dusty fluid. The flow and heat transfer of dusty fluids in a channel are extremely useful in improving the design and operation of many industrial and engineering devices. The phenomenon of flow and heat transfer in dusty fluids in two parallel plates has been analyzed by many researchers. Saffman [23] discussed on the stability of laminar flow of a dusty gas. Flow of a dusty gas through a channel with arbitrary time varying pressure gradient has been analyzed by Gupta and Gupta [24]. Unsteady flow of a conducting dusty fluid through a rectangular channel with time dependent pressure gradient has been studied by Singh [25]. Further Prasad and Ramacharyulu [26] investigated the unsteady flow of a dusty incompressible fluid between two parallel plates under an impulsive pressure gradient. Attia [27] studied the influence of temperature dependent viscosity on MHD channel flow of dusty fluid with heat transfer. Attia [28] discussed the unsteady MHD flow and heat transfer of dusty fluid between parallel plates with variable physical properties. Influence of temperaturedependent viscosity on the MHD Couette flow of dusty fluid with heat transfer have been also studied by Attia [29]. Palani and Ganesan [30] explored the heat transfer effect on dusty gas flow past a semi infinite inclined plate. Makinde and Chinyoka [31] worked on MHD transient flows and heat transfer of dusty fluid in a channel with variable physical properties and Navier slip condition. Heat transfer in MHD oscillatory flow of dusty fluid in a rotating porous vertical channel has been investigated by Chand et.al. [33]. Attia et.al. [34]discussed the MHD flow of a dusty fluid between two infinite parallel plates with temperature dependent physical properties under exponentially decaying pressure gradient. Jalil et.al. [35] discussed an exact solution of MHD boundary layer flow of dusty fluid over a stretching surface.

Motivated by above studies we propose to study the problem of unsteady hydromagnetic oscillatory flow and heat transfer in an electrically conducting incompressible, dusty viscoelastic fluid through porous medium in an inclined channel in the presence of magnetic field, thermal radiation and heat source/sink effect.

Mathematical Formulation of the problem

Consider an unsteady free convective flow of an incompressible, electrically conducting, radiating, dusty viscoelastic, fluid through a porous inclined channel under the effect of transversely applied magnet field of constant strength. The coordinate system is considered with x-axis along the centre of the channel and y-axis perpendicular to it. The following assumptions have been made

1. A uniform magnetic field is applied normal to the planes of the plates.

- 2. Boussinesq approximation is applied.
- 3. The dust particles are spherical in shape are uniformly distributed.
- 4. The magnetic Reynolds number is assumed to be very small so that the induced magnetic field may be neglected.
- 5. The plates of the channel is assumed to be non conducting and kept at two different temperature.
- 6. The initial temperature of the fluid and the dust particle is assumed to be the same.
- 7. The heat due to viscous dissipation and Joule heating has been neglected.
- 8. The size of the dust particle has be assumed to be large as compare to the pore size of the channel.

The channel plate are considered to be infinitely long and the problem under consideration is one dimensional with velocity of fluid and dust particles as the function of the space coordinate y^* and time t*. Under the above assumptions, the flow equations proposed by Walter [12], for the fluid known as Walter's liquid-B for viscoelastic fluid and following Chand and Kumar[32]. The governing equations in case one dimensional takes the form



Figure.1. Geometrical interpretation of the problem.

Equation of continuity

$$\frac{\partial \mathbf{v}^*}{\partial \mathbf{y}^*} = \mathbf{0}, \Longrightarrow \mathbf{v}^* = \text{constant}$$
 (1)

Equation of motion

$$\frac{\partial u^{*}}{\partial t^{*}} = -\frac{1}{\rho} \frac{\partial p^{*}}{\partial x^{*}} + v \frac{\partial^{2} u^{*}}{\partial y^{*2}} - \frac{k_{0}}{\rho} \left(\frac{\partial^{3} u^{*}}{\partial y^{2*} \partial t^{*}} \right) + \frac{k_{1} N_{1}}{\rho} \left(u^{*}_{p} - u^{*} \right) - \frac{v}{K^{*}} u^{*} + g\beta (T^{*} - T_{1}^{*}) \sin\alpha - \frac{\sigma B_{0}^{2} u^{*}}{\rho},$$

$$m_{p} \frac{\partial u^{*}_{p}}{\partial t^{*}} = K_{1} N_{1} \left(u^{*} - u^{*}_{p} \right),$$
(2)

The boundary conditions relevant to the problem are

$$\begin{array}{l} \text{at } y^{*} = 0 : u^{*} = u_{p}^{*} = 0 \text{, } T^{*} = T_{p}^{*} = 0 \text{,} \\ \text{at } y^{*} = d : u^{*} = u_{p}^{*} = U_{0} \big(1 + \epsilon e^{i\omega^{*}t^{*}} \big) \text{,} \\ T^{*} = T_{F}^{*} + \epsilon (T_{F}^{*} - T_{0}^{*}) e^{i\omega^{*}t^{*}} \end{array} \right)$$
(6).

Using Cogley et.al.[36], the radiative heat flux term q^{*} is given by $\frac{\partial q^*}{\partial y^*} = 4\alpha^2 (T^* - T_0^*).$ (7) (4)

Where u^{*} is the velocity of the fluid, u^{*}_p is the velocity of the dust particles, T^{*} is the temperature of the fluid, T^{*}_p is the temperature of the dust particles, c_p is the specific heat capacity of the fluid at constant pressure, c_s is the specific heat capacity of the dust particles, k is the thermal conductivity of the fluid, q^{*} is the radiative heat flux, Q^{*} is the heat absorption coefficient, $\gamma_T = \frac{3P_T\gamma_P c_s}{2c_p}$ is the temperature relaxation time, $\gamma_P = \frac{2\rho_P d^2}{9\rho_V}$ is velocity relaxation time

and $P_r = \frac{v \rho C_p}{k}$ is the Pradntl Number.

Introducing the following non-dimensional quantities

$$\begin{aligned} x, y &= \frac{x^*, y^*}{d}, u = \frac{u^*}{U_0}, u_p = \frac{u_p^*}{U_0}, \omega = \frac{d\omega^*}{U_0}, t = \frac{t^*U_0}{d}, \theta = \frac{T^* - T_0^*}{T_F^* - T_0^*}, \theta_p = \frac{T_p^* - T^*}{T_F^* - T_0^*}, R_e = \frac{U_0 d}{\nu}, H = \frac{\nu m_p}{k_1 d^2}, P_r = \frac{\nu \rho C_p}{k}, R = \frac{k_1 N_1 d^2}{\rho \nu}, R = \frac{d^2 \sigma R_0^2}{k}, R = \frac{d^2 \sigma R$$

Using above non-dimensional quantities, the governing equations reduces to

$$R_{e}\frac{\partial u}{\partial t} = -\frac{\partial P}{\partial x} + \frac{\partial^{2} u}{\partial y^{2}} + R_{e}K_{v}\frac{\partial^{3} u}{\partial y^{2}\partial t} + R(u_{p} - u) - (M^{2} + K_{p})u + G_{r}\sin\alpha,$$
(8)

$$HR_{e}\frac{\partial u_{p}}{\partial t} = u - u_{p}, \qquad (9)$$

$$R_e P_r \frac{\partial T}{\partial t} = \frac{\partial^2 u}{\partial y^2} - (N^2 + Q)T + \frac{2R}{3} (T_p - T), \qquad (10)$$

$$\frac{\partial T_{p}}{\partial t} = -L_{0} (T_{p} - T), \qquad (11)$$

And the corresponding boundary conditions in non dimensional form are

$$\begin{array}{l} \text{at } y = 0 : u = u_p = 0 \text{, } T = T_p = 0 \text{,} \\ \text{at } y = 1 \quad : u = u_p = 1 + \epsilon e^{i\omega t} \text{,} \\ T = T_p = 1 + \epsilon e^{i\omega t} \end{array} \right\}$$
(12)

Method of solution

Following Sengupta and Ahmed [37], we assume the solution of the form

$$\begin{array}{l} u(y,t) = u_0(y) + \epsilon e^{i\omega t} u_1(y) + o(\epsilon^2) \\ u_p(y,t) = \psi_0(y) + \epsilon e^{i\omega t} \psi_1(y) + o(\epsilon^2) \\ T(y,t) = T_0(y) + \epsilon e^{i\omega t} T_1(y) + o(\epsilon^2) \\ T_p(y,t) = \xi_0(y) + \epsilon e^{i\omega t} \xi_1(y) + o(\epsilon^2) \\ - \frac{\partial P}{\partial x} = A(1 + \epsilon e^{i\omega t}) \end{array} \right\},$$
(13)

The zero order equations are given by the following expression

$$\frac{\partial^{2} u_{0}}{\partial y^{2}} - (M^{2} + K_{p})u_{0} + R(\psi_{0} - u_{0}) = -G_{r} \sin \alpha - A,(14) \qquad u_{0} - \psi_{0} = 0$$

$$0(15) \qquad \qquad \frac{\partial^{2} T_{0}}{\partial y^{2}} - (N^{2} + Q)T_{0} - \frac{2R}{3}(\xi_{0} - T_{0}) = 0,(16)$$

$$\xi_{0} - T_{0} = 0,(17) \qquad The transformed boundary conditions$$

at
$$y = 0$$
: $u_0 = \psi_0 = 0$, $T_0 = \xi_0 = 0$,
at $y = 1$: $u_0 = \psi_0 = 1$, $T_0 = \xi_0 = 1$ }.(18)
given by the following expression

$$\frac{\partial^2 u_1}{\partial y^2} - \frac{i\omega}{1 + i\omega R_e K_v} \Big[\frac{HRR_e}{1 + i\omega HR_e} + \frac{M^2 + K_p}{i\omega} + R_e \Big] u_1 = \frac{-G_r \sin \alpha - A}{1 + i\omega R_e K_v}, (19)$$
(1 +
 $i\omega R_e H)\psi_1 = u_1, (20)$
 $\Big\{ (N^2 + Q) - i\omega \Big(\frac{2R}{3(L_0 + i\omega)} + R_e P_r \Big) \Big\} T_1 = 0, (21)$
 $L_0 T_1, (22)$
Subjected to the

transformed boundary conditions

at
$$y = 0 : u_1 = \psi_1 = 0$$
, $T_1 = \xi_1 = 0$,
at $y = 1 : u_1 = \psi_1 = 1$, $T_1 = \xi_1 = 1$. (23)
the zero order equations (14) to (17) under the boundary conditions (18) are obtained in the following form

$$u_{0} = A_{3}e^{a_{3}y} + B_{3}e^{-a_{3}y} + X_{1}e^{a_{1}y} + Y_{1}e^{-a_{1}y} + Z_{1}, \qquad (24)$$

$$\psi_{0} = u_{0},(25)$$

$$A_{1}e^{a_{1}y} + B_{1}e^{-a_{1}y}, \qquad (26)$$

 $\xi_0 = T_0$,(27)

solutions of the first order equations from (19) to (22) under the boundary conditions (23) are obtained and can be listed as below

$$\begin{split} u_1 &= A_4 e^{a_4 y} + B_4 e^{-a_4 y} + X_2 e^{a_2 y} + Y_2 e^{-a_2 y} + Z_2, (28) \\ &\qquad \qquad \psi_1 = \\ \frac{u_1}{(1 + i \omega R_e H)}, (29) \\ B_2 e^{-a_2 y}, (30) \end{split}$$

$$\xi_1 = \left(\frac{L_0}{L_0 + i\omega}\right) T_1(31)$$
The solutions of the

equations (8) to (11) under the boundary conditions (12) are finally obtained the expression for the fluid velocity, dust particle velocity, fluid temperature and dust particle temperature obtained as below.

$$u = (A_3 e^{a_3 y} + B_3 e^{-a_3 y} + X_1 e^{a_1 y} + Y_1 e^{-a_1 y} + Z_1) + \varepsilon e^{i\omega t} (A_4 e^{a_4 y} + B_4 e^{-a_4 y} + X_2 e^{a_2 y} + Y_2 e^{-a_2 y} + Z_2),$$
(32)

$$u_{p} = (A_{3}e^{a_{3}y} + B_{3}e^{-a_{3}y} + X_{1}e^{a_{1}y} + Y_{1}e^{-a_{1}y} + Z_{1}) + \frac{\varepsilon e^{i\omega t}}{(1+i\omega R_{e}H)}(A_{4}e^{a_{4}y} + B_{4}e^{-a_{4}y} + X_{2}e^{a_{2}y} + Y_{2}e^{-a_{2}y} + Z_{2}),$$
(33)

$$T = (A_1 e^{a_1 y} + B_1 e^{-a_1 y}) + \varepsilon e^{i\omega t} (A_2 e^{a_2 y} + B_2 e^{-a_2 y}), \quad (34)$$

$$T_{p} = (A_{1}e^{a_{1}y} + B_{1}e^{-a_{1}y}) + \varepsilon e^{i\omega t} \left(\frac{L_{0}}{L_{0} + i\omega}\right) (A_{2}e^{a_{2}y} + B_{2}e^{-a_{2}y}),$$
(35)

The significant physical quantities of importance are as follows:

Skin friction coefficient(τ) for fluid velocity and dust particle velocity at the lower plate of the channel are:

$$\tau = \left(\frac{\partial u}{\partial y}\right)_{y=0}$$

The

$$\begin{aligned} \tau &= [a_{3}(A_{3} - B_{3}) + a_{1}(X_{1} - Y_{1})] + \varepsilon e^{i\omega t} [a_{4}(A_{4} - B_{4}) + a_{2}(X_{2} - Y_{2})], \\ (36) \\ \tau_{p} &= \left(\frac{\partial u_{p}}{\partial y}\right)_{y=0} \\ \tau_{p} &= [a_{3}(A_{3} - B_{3}) + a_{1}(X_{1} - Y_{1})] + \frac{\varepsilon e^{i\omega t}}{(1 + i\omega R_{e}H)} [a_{4}(A_{4} - B_{4}) + a_{2}(X_{2} - Y_{2})], \\ (37) \\ \tau &= \left(\frac{\partial u}{\partial y}\right)_{y=1} \\ \tau &= [a_{3}(A_{3}e^{a_{3}} - B_{3}e^{-a_{3}}) + a_{1}(X_{1}e^{a_{1}} - Y_{1}e^{-a_{1}})] + \varepsilon e^{i\omega t} [a_{4}(A_{4}e^{a_{4}} - B_{4}e^{-a_{4}}) + a_{2}(X_{2}e^{a_{2}} - Y_{2}e^{-a_{2}})], \\ (38) \\ \tau_{p} &= \left(\frac{\partial u_{p}}{\partial y}\right)_{y=1} \\ \tau_{p} &= [a_{3}(A_{3}e^{a_{3}} - B_{3}e^{-a_{3}}) + a_{1}(X_{1}e^{a_{1}} - Y_{1}e^{-a_{1}})] + \frac{\varepsilon e^{i\omega t}}{(1 + i\omega R_{e}H)} [a_{4}(A_{4}e^{a_{4}} - B_{4}e^{-a_{4}}) + a_{2}(X_{2}e^{a_{2}} - Y_{2}e^{-a_{2}})], \\ (39) \end{aligned}$$

Nusselt Number (Nu) for fluid temperature and dust particle temperature at the lower plate of the channel are:

$$\begin{split} \mathrm{Nu} &= \left(\frac{\partial \mathrm{T}}{\partial \mathrm{y}}\right)_{\mathrm{y}=0} \\ \mathrm{Nu} &= [\mathrm{a}_{1}(\mathrm{A}_{1} - \mathrm{B}_{1})] + \varepsilon \mathrm{e}^{\mathrm{i}\omega \mathrm{t}} [\mathrm{a}_{2}(\mathrm{A}_{2} - \mathrm{B}_{2})], \quad (40) \\ \mathrm{Nu}_{\mathrm{p}} &= \left(\frac{\partial \mathrm{T}_{\mathrm{p}}}{\partial \mathrm{y}}\right)_{\mathrm{y}=0} \\ \mathrm{Nu}(\mathrm{p}) &= [\mathrm{a}_{1}(\mathrm{A}_{1} - \mathrm{B}_{1})] + \varepsilon \mathrm{e}^{\mathrm{i}\omega \mathrm{t}} \left(\frac{\mathrm{L}_{0}}{\mathrm{L}_{0} + \mathrm{i}\omega}\right) [\mathrm{a}_{2}(\mathrm{A}_{2} - \mathrm{B}_{2})], (41) \\ \mathrm{Nu} &= [\mathrm{a}_{1}(\mathrm{A}_{1} \mathrm{e}^{\mathrm{a}_{1}} - \mathrm{B}_{1} \mathrm{e}^{\mathrm{a}_{1}}) -] + \varepsilon \mathrm{e}^{\mathrm{i}\omega \mathrm{t}} [\mathrm{a}_{2}(\mathrm{A}_{2} \mathrm{e}^{\mathrm{a}_{2}} - \mathrm{B}_{2} \mathrm{e}^{-\mathrm{a}_{2}})], \quad (42) \\ \mathrm{Nu}_{\mathrm{p}} &= \left(\frac{\partial \mathrm{T}_{\mathrm{p}}}{\partial \mathrm{y}}\right)_{\mathrm{y}=1} \\ \mathrm{Nu}(\mathrm{p}) &= [\mathrm{a}_{1}(\mathrm{A}_{1} \mathrm{e}^{\mathrm{a}_{1}} - \mathrm{B}_{1} \mathrm{e}^{\mathrm{a}_{1}}) -] + \varepsilon \mathrm{e}^{\mathrm{i}\omega \mathrm{t}} \left(\frac{\mathrm{L}_{0}}{\mathrm{L}_{0} + \mathrm{i}\omega}\right) [\mathrm{a}_{2}(\mathrm{A}_{2} \mathrm{e}^{\mathrm{a}_{2}} - \mathrm{B}_{2} \mathrm{e}^{-\mathrm{a}_{2}})], \quad (43) \end{split}$$

The all constant used above have been list in the appendix.

Results and discussions:

The following discussion brings out the effect of the pertinent parameters such as permeability parameter (K_p), magnetic field parameter (M), radiation parameter (N) and angle of inclination (α) on the fluid and dust particle velocity. Figure 2 & 6, 3 & 7 and 4 & 8 shows the effect of permeability parameter (K_p), magnetic field parameter (M) and radiation parameter (N) on fluid velocity and dust particle velocity, both the fluid velocity and dust particle velocity decreases with the increasing values of permeability parameter (K_p), magnetic field parameter (M) and radiation parameter (N). The effect of angle of inclination (α) on fluid velocity and dust particle velocity has been obtained in figures 5 & 9. The fluid and dust particle velocity increases with the increase in angle of inclination(α).



Figure.2. Fluid velocity variation for different values of permeability parameter (K_p).



Figure.3. Fluid velocity variation for different values of magnetic field parameter (M).



Figure.4. Fluid velocity variation for different values of Hartmann number(N).



Figure.5. Fluid velocity variation for different values of angle (α).



Figure.6. Dust particle velocity variation for different values of permeability parameter (K_p).



Figure.7. Dust particle velocity variation for different values of magnetic field parameter (M).



Figure.8. Dust particle velocity variation for different values of radiation parameter (N).



Figure.9. Dust particle velocity variation for different values of angle (α).

Tables 1 to 4 expresses numerically the influence of various parameters like heat sink parameter (Q), coefficient of skin friction (τ) and Nusselt number (Nu) for both fluid and dust particle velocity. It is evident from table 1 & 2 that both fluid and dust particle velocities decreases with the increase in heat sink parameter (Q). Table 3 & 4 expresses numerically the variation of fluid and dust particle velocity with frequency of oscillations(ω). From these tables we observed that with the increase in frequency of oscillations(ω), both the fluid and dust particle velocities decreases and after certain value of oscillations there is repetition of both the fluid and dust particle velocities.

Significant physical quantities of importance are shown by table 5 & 6. Table 5 & 6 shows the results for skin friction coefficient (τ) and Nusselt number (Nu) with magnetic field parameter (M) and radiation parameter (N) respectively at y = 0 and y = 1. Table 5 depicts that with the increase in magnetic field parameter (M), Skin friction coefficient(τ) decreases for both fluid velocity and dust particle velocity at y = 0, and the reverse pattern is obtained for both fluid and dust particle velocity at y = 1. It is seen from table 6 that with the increase in radiation parameter (N), the Nusselt number (Nu) decreases for both fluid velocity and dust particle velocity at y = 0, and increases at y = 1.

Table.1. Fluid velocity for different values of heat sink parameter (Q).

Q	0	0.2	0.4	0.6	0.8	1
0	0	0.21200	0.41526	0.61272	0.80696	1.0001
1	0	0.21112	0.41381	0.61123	0.80602	1.0001
3	0	0.20962	0.41129	0.60857	0.80428	1.0001
5	0	.020848	0.40937	0.60652	0.80291	1.0001

Q	0	0.2	0.4	0.6	0.8	1
0	0	0.21198	0.41523	0.61268	0.80690	1
1	0	0.21111	0.41378	0.61119	0.80569	1
3	0	0.20960	0.41126	0.60853	0.80422	1
5	0	0.20847	0.40934	0.60647	0.80285	1

Table.2.Dust particles velocity for different values of heat sink parameter (Q).

Table.3. Fluid velocity for different values of frequency of oscillations (ω)

^y / _ω	0	0.2	0.4	0.6	0.8	1
1	0	0.21182	0.41497	0.61244	0.80678	1
10	0	0.21179	0.41490	0.61233	0.80663	1
20	0	0.21182	0.41497	0.61244	0.80678	1

Table.4. Fluid velocity for different values of frequency of oscillations (ω)

^y / _ω	0	0.2	0.4	0.6	0.8	1
1	0	0.21181	0.41494	0.61239	0.80672	1
10	0	0.21180	0.41492	0.61238	0.80671	1
20	0	0.21181	0.41494	0.61238	0.80671	1

Table.5. Skin friction coefficient(τ):

М	0	0.2	0.5	0.7
$\tau_{y=0}$	1.1703	1.1355	1.0863	1.0552
$\tau_{py=0}$	1.1702	1.1352	1.0862	1.0551
$\tau_{y=1}$	0.80014	0.86807	0.96676	1.0305
$\tau_{py=1}$	0.80006	0.86799	0.96667	1.0304

Table.6. Nusselt Number (Nu):

N	0	1	3	5	7
Nu(y = 0)	0.96752	0.82492	0.29288	0.066321	0.012612
Nu(p)(y = 0)	0.96752	0.82492	0.29288	0.066321	0.012612
Nu(y = 1)	1.0659	1.3714	3.0476	5.0209	7.0150
Nu(p)(y = 1)	1.0659	1.3714	3.0476	5.0209	7.0150

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